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(54) Process for the Production of Titanium Dioxide

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A process the production of titanium dioxide

Abstract of the Disclosure

The present invention relates to a process for the production of titanium dioxide by discontinuous digestion of titanium slag with sulphuric acid, production of a titanyl sulphate solution suitable for hydrolysis from the solid digestion cake obtained during digestion, hydrolysis of the titanyl sulphate, separation and calcination of the titanium-containing hydrolyzate, evaporation of the waste acid separated from the hydrolyzate and re-use of the sulphuric acid separated from the evaporated waste acid in the digestion of titanium slag.

A process for the production of titanium dioxide

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10 The present invention relates to a process for the
production of titanium dioxide by discontinuous digestion
of titanium slag with sulphuric acid, production of a
titanyl sulphate solution suitable for hydrolysis from the
solid digestion cake obtained during digestion, hydrolysis
15 of the titanyl sulphate, separation and calcination of the
titanium-containing hydrolyzate, evaporation of the waste
acid separated from the hydrolyzate and re-use of the
sulphuric acid separated from the evaporated waste acid
in the digestion of titanium slag.

20 The requirement for recycling of sulphuric acid from
the TiO_2 production process by the sulphate process is
having to be met more and more. In addition to the
expected economic disadvantages in comparison with dumping
of waste acid in the ocean, the process often encounters
technical problems.

25 A process for working up waste acids is known from
DE-A 3 327 769 and is adopted on an industrial scale. De-
pending on the local condition, however, problems can
arise here if the waste acid is to be almost completely
recycled.

30 According to the working up process currently
adopted, the waste acid is concentrated, preferably by
multi-stage vacuum evaporation, until a 60 to 70%
sulphuric acid with a low content of dissolved metal
sulphates can be separated by filtration from crystal-
lized metal sulphates.

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Le A 23 707

5 The concentration of this recovered sulphuric acid
is generally too low, however, to produce a sulphuric acid
initial concentration suitable for the discontinuous
digestion of raw material when mixed with fresh sulphuric
acid or oleum, which is required for replacing the sul-
phuric acid losses (by metal sulphate binding, residual
10 moisture in the separated metal sulphates, waste water).
It is therefore necessary further to evaporate the sul-
phuric acid separated from the metal sulphates, and this
can be effected, for example, by using the waste heat from
TiO₂ calcination (EP-A 97 259).

15 The greater the content of recycled sulphuric acid
in the total mixture, the higher the concentration of the
recycled acid must be. As the concentration increases,
however, the requirements in energy and equipment also
increase. In particular, when using the titanium slags
20 which are advantageous from an ecological point of view
as raw material, a particularly high concentration of the
recycled acid is required if maximum possible industrial
recycling is desired.

25 A more desirable situation arises if the relatively
low sulphuric acid losses during digestion of the titanium
slags can be replaced by 95 to 98% sulphuric acid ("fresh
acid") instead of oleum. The production of oleum can thus
be omitted.

30 In this case, according to the prior art it is only
possible to concentrate recycling acid in a high concen-
tration apparatus (for example a Pauling distillation
vessel) to about 96% (Ullmanns Encyklopädie d. techn.
Chemie, 4th edition, volume 18, page 579, Verlag Chemie,

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5 Weinheim 1979). However, this stage of the process is extremely expensive with respect both to the investment costs and to the energy and maintenance costs.

It is accordingly the object of the present invention to propose a method which overcomes the above-mentioned disadvantages of the prior art in an economical manner.

10 This object can surprisingly be achieved by the following combination of measures:

- evaporation of the 60 to 75% sulphuric acid separated from the metal sulphates and containing dissolved metal sulphates under vacuum in horizontal or circulation evaporators at from 120 to 190°C to 76 to 87% H_2SO_4 (based on salt-free sulphuric acid),
- 15 mixing of the ground titanium slag with 95 to 98% sulphuric acid at from 30 to 80°C and addition of the recycled acid at a temperature of from 80 to 190°C, preferably from 100 to 160°C.

The present invention accordingly relates to a process for the production of titanium dioxide by discontinuous digestion of titanium slag with sulphuric acid, production of a titanyl sulphate solution suitable for hydrolysis from the solid digestion cake obtained during digestion, hydrolysis of the titanyl sulphate, separation and calcination of the titanium-containing hydrolyzate, evaporation of the waste acid separated from the hydrolyzate and re-use of the sulphuric acid separated from the evaporated waste acid in titanium slag digestion, a 60 to 75% pre-concentrated sulphuric acid being separated from the solid metal sulphates and hydrogen sulphates after

5 evaporation of the waste acid, this sulphuric acid being
further evaporated under vacuum to a concentration of
between 76 to 87% H_2SO_4 (calculated as salt-free sulphuric
acid) and being used together with 95 to 98% sulphuric
acid in the digestion of the ground titanium slag.

10 The invention also teaches the conditions under which
the titanium slag is to be digested in order to keep the
necessary concentration of the recycled sulphuric acid and
therefore the costs of sulphuric acid concentration as low
as possible.

15 The titanium slag is advantageously mixed with warm
95 to 98% sulphuric acid ("fresh acid") at from 30 to
80°C, preferably from 50 to 80°C.

20 Digestion is initiated by addition of the uncooled
or slightly cooled recycled acid, supplied from sulphuric
acid evaporation to the warm fresh acid/slag mixture. The
process corresponding to the prior art involving ini-
tiating digestion by addition of water or introduction of
steam would require a substantially higher concentration
of the recycled acid than the process according to the
invention.

25 A particularly preferred embodiment of the process
according to the invention therefore involves initiating
the digestion reaction by addition of hot 76 to 87%
sulphuric acid ("recycled acid") at from 80 to 190°C,
preferably from 100 to 160°C.

30 A further reduction in the minimum sulphuric acid
concentration required for discontinuous slag digestion
by 2 to 3%, without losses of TiO_2 yield occurring, is
successful because steam is blown through the digestion
cake instead of air during the maturing time once the
35 maximum reaction temperature has been reached.

5 In a particularly desirable embodiment of the process according to the invention, the concentration of the sulphuric acid is advantageously between 87 and 91%, preferably 88 and 90% H_2SO_4 (calculated as solids-free and salt-free acid) at the start of the digestion reaction and
10 from 35 to 70% of the required sulphuric acid is recovered as recycled acid from the process.

The necessary temperatures of the fresh acid and the recycled acid can be lowered according to the invention by grinding the titanium slag more finely.

15 The production of the 76 to 87% acid from 60 to 75% pre-concentrated sulphuric acid is preferably carried out by evaporation at from 120 to 190°C and from 40 to 150 mbar.

20 Horizontal evaporators with tantalum heat exchangers or circulation evaporators are particularly suitable for these evaporation processes not only for reasons of energy consumption.

25 Valuation of the process according to the invention has to consider the fact that secondary energy can be used instead of primary energy for producing the recycled acid and that the investment and maintenance costs are substantially lower compared with the prior art.

The drawing serves to illustrate the process according to the invention.

30 The fresh acid (1) required for the digestion of raw material is mixed in the digestion reactor (3) or in a preceding mixer with the ground titanium slag (2) (optionally with addition of ground ilmenite). The fresh acid should have a temperature of from 30 to 80°C,
35 preferably from 50 to 80°C. The necessary quantity of

5 recycled acid (17) is introduced at a temperature of from
80 to 190°C, preferably from 100 to 160°C, into the
digestion reactor (3) while blowing air through the
mixture present and the exothermal reaction is thus
initiated. If steam (4) which is at least 150°C hot is
10 blown in instead of air once the maximum reaction temperature has been attained, the temperature drop of the
digestion mixture can be reduced and the TiO₂ yield
improved. After a maturing time of from 5 to 8 hours,
after which, from experience, no further improvement in
the TiO₂ yield can be expected, the digestion cake is
15 dissolved with water or preferably with sulphuric acid-
containing waste water (5) from the TiO(OH)₂ hydrolyzate
filtration process.

The titanyl sulphate solution is prepared in known
manner for hydrolysis. During the hydrolysis process (6),
20 sulphuric acid-containing waste water (5) is preferably
used as diluent water. The hydrolyzate (8) is calcined in
known manner to titanium dioxide (10).

The metal sulphate-containing sulphuric acid (waste
acid) (11) produced during filtration (7) normally has a
25 concentration of from 20 to 27% H₂SO₄. It can be pre-
evaporated using process heat before being evaporated in
known manner in an evaporator which is preferably a
multistage vacuum evaporator (12) until most of the metal
sulphates are crystallized and a 60 to 75% sulphuric acid
30 remains (= evaporation 1).

After cooling the suspension supplied from the
evaporation I to from 40 to 70°, the metal sulphates (14)
are separated from the sulphuric acid, preferably by
35 filtration (13).

5 The metal sulphates are partly in the form of
hydrogen sulphates and contain 60 to 75% sulphuric acid
as moisture. It is therefore advantageous to decompose
this "filter salt" thermally with formation of SO_2 and to
10 produce therefrom the 95 to 98% sulphuric acid required
as fresh acid. However, reaction with Ca compounds (DE-A
3 327 770) or a different harmless elimination process is
also possible.

15 Sulphuric acid losses occur mainly through the filter
salt, but also through the moisture of the solid residues
resulting from raw material digestion, the sulphuric acid
bound in the $\text{TiO}(\text{OH})_2$ and the unavoidable waste water. As
pre-concentrated acid, therefore, only about 40 to 60% of
the sulphuric acid used during digestion can be recovered.
With 60 to 75% H_2SO_4 , however, the concentration of this
20 acid is too low to allow autothermal slag digestion in
mixture with the necessary amount of from 95 to 98% fresh
acid.

25 The pre-concentrated acid (15) which still contains
about 3 to 6% by weight of dissolved metal sulphates
therefore must be evaporated in an evaporation II (16) to
76 to 87% H_2SO_4 (as salt-free acid), before it can be
recycled (17) for the digestion of the raw material. The
evaporation II (16) is carried out according to the inven-
30 tion by vacuum evaporation at 120 to 190°C. Circulation
evaporators or horizontal evaporators with tantalum heat
exchangers can be used as evaporator systems. Horizontal
evaporators are preferred owing to the particularly high
specific evaporation capacity (with respect to the
tantalum heat exchanger surface). Preheating of the pre-
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5 concentrated sulphuric acid almost to boiling point is
advantageous (at a given evaporation pressure). Steam-
heated graphite heat exchangers are preferred for the
preheating operation. Cooling of the recycled acid
10 supplied from the evaporator is omitted or is optionally
carried out using the pre-concentrated acid introduced as
a cooling liquid, only until the temperature of the
recycled acid is still sufficient to initiate the di-
gestion reaction in the manner described above, i.e. until
the temperature lies in the range of from 80 to 190°C.

15 A substantial advantage of the process according to
the invention lies in the fact that problems which arise
during further cooling of this acid are avoided by using
the recycled acid at a temperature of from 80 to 190°C
because the metal sulphates dissolved in that acid (about
4 to 7% by weight) crystallize in an extremely finely
20 divided form at lower temperatures. As these salts tend
to settle on cool surfaces, they lead to frequent inter-
ruptions in the operation. These problems can be avoided
by introducing the recycled acid at a temperature at which
the dissolved metal sulphates not yet crystallize.

25 The process according to the invention, which is
substantially more economical than conventional high
concentration processes according to the prior art
evaporating sulphuric acid to about 96% H_2SO_4 and
initiating the digestion reaction by introduction of
30 steam into the sulphuric acid-slag mixture will be
described with reference to the following non-limiting
Examples.

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Le A 23 707

Example 1 (Comparison Example)

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17.5 t of ground titanium slag were mixed with 18 t of metal sulphate-containing recycled acid and with 13.6 t of fresh 96% sulphuric acid (20°C). The digestion reaction was initiated by addition of 1.4 t of water and introduction of 0.6 t of steam. The maximum reaction temperature of 203°C was attained after 10 minutes. After initiation of the reaction, air was blown through the mixture (for 30 minutes at 350 m³_n/h, then for 7 hours at 20 m³_n/h). After a maturing time of 7 hours, the digestion cake had a temperature of 169°C. The TiO₂ yield was 95.3%.

The digestion cake was dissolved with a proportion of the sulphuric acid-containing waste water from the hydrolyzate filtration (5.4% by weight H₂SO₄). After working up the titanyl sulphate solution, the mixture was hydrolysed using a further proportion of the sulphuric acid-containing waste water as diluent water.

85 t of waste acid containing 23.2% H₂SO₄ and 29.8% SO₄²⁻ (total) were separated from the hydrolyzate filtration process. The waste acid was evaporated in a 2-stage vacuum evaporator until the sulphuric acid (calculated as salt-free acid) had a concentration of 66% H₂SO₄. 31 t of 5 bar steam were used up for evaporating 47.5 t of H₂O.

11.3 t of sulphuric acid-containing filter cake were separated from the metal sulphate-sulphuric acid suspension after cooling to 55°C. The pre-concentrated acid (25.7 t) contained 62.8% of H₂SO₄, 32.4% of H₂O and 4.8% of dissolved metal sulphates.

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Le A 23 707

5 introduced had a temperature of 89°C and the discharged
recycled acid had a temperature of 145°C . Only 4.94 t of
10 H_2O had to be evaporated instead of 5.7 t of H_2O . The
total energy consumption for the production of the
recycled acid from pre-concentrated acid and the blowing
of steam through the digestion cake was 19,460 kJ in
comparison with 22,700 kJ in Example 2.

Example 4

15 Laboratory experiments were carried out to examine
how the temperature of the recycled acid can be lowered
without problems arising due to an excessively slow rate
of the digestion reaction. 500 g of slag ground to varying
finenesses were mixed with 520 g of 96% sulphuric acid and
preheated to the temperature T_1 . The mixture was then
20 mixed in an insulated vessel with 590 g of pure 85% sul-
phuric acid having a temperature of T_2 . The mixture was
stirred while introducing 250 l of air/h and the temper-
ature gradient was recorded. The experimental results are
compiled in Table 1. T_3 is the temperature of the mixture
after addition of the 85% sulphuric acid and T_4 the
25 maximum temperature attained. t is the time period until
the maximum temperature is attained after addition of the
85% acid.

Table 1

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Exp. No.	Fineness of grinding		T ₁	T ₂	T ₃	T ₄	t
	% by weight	<40 μm	[°C]	[°C]	[°C]	[°C]	[min]
10	1	81	50	110	76	-	-
	2	81	50	140	91	106	36
	3	81	70	140	101	154	67
	4	81	80	140	109	193	37
	5	81	70	160	117	192	23
15	6	100	50	120	86	168	42
	7	100	50	140	95	185	28

20 The experimental results show that the temperature of the recycled acid can be lower if the titanium slag is ground more finely (Experiment 7) than with a coarser grinding (Experiment 2) achieving approximately the same reaction rate. Also the temperature of the 96% fresh acid can obviously be lowered instead of the temperature of the recycled acid.

25 The slower rise in the temperature of the laboratory digestions in comparison with the rise in temperature on an industrial scale is due to the relatively high thermal losses.

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Le A 23 707

THE EMBODIMENTS OF THE INVENTION IN WHICH AN EXCLUSIVE PROPERTY OR PRIVILEGE IS CLAIMED ARE DEFINED AS FOLLOWS:

1. A process for the production of titanium dioxide by discontinuous digestion of titanium slag with sulphuric acid, the production of a titanyl sulphate solution suitable for hydrolysis from the solid digestion cake obtained during digestion, hydrolysis of the titanyl sulphate, separation and calcination of the titanium-containing hydrolyzate, evaporation of the waste acid separated from the hydrolyzate and re-use of the sulphuric acid separated from the evaporated waste acid in the digestion of titanium slag, characterized in that, after evaporation of the waste acid from the solid metal sulphates and hydrogen sulphates, a 60 to 75% pre-concentrated sulphuric acid is separated and is further evaporated under vacuum to a concentration of between 76 and 87% H_2SO_4 (calculated as salt-free sulphuric acid) and is used together with 95 to 98% sulphuric acid in the digestion of the ground titanium slag.
2. A process according to claim 1, wherein the titanium slag is mixed with warm 95 to 98% sulphuric acid ("fresh acid") at from 30 to 80°C.
3. A process according to claim 2, wherein the fresh acid is mixed at from 50 to 80°C.
4. A process according to claim 1, 2 or 3, wherein the digestion reaction is initiated by addition of hot 76 to 87% sulphuric acid ("recycled acid") at from 80 to 190°C.

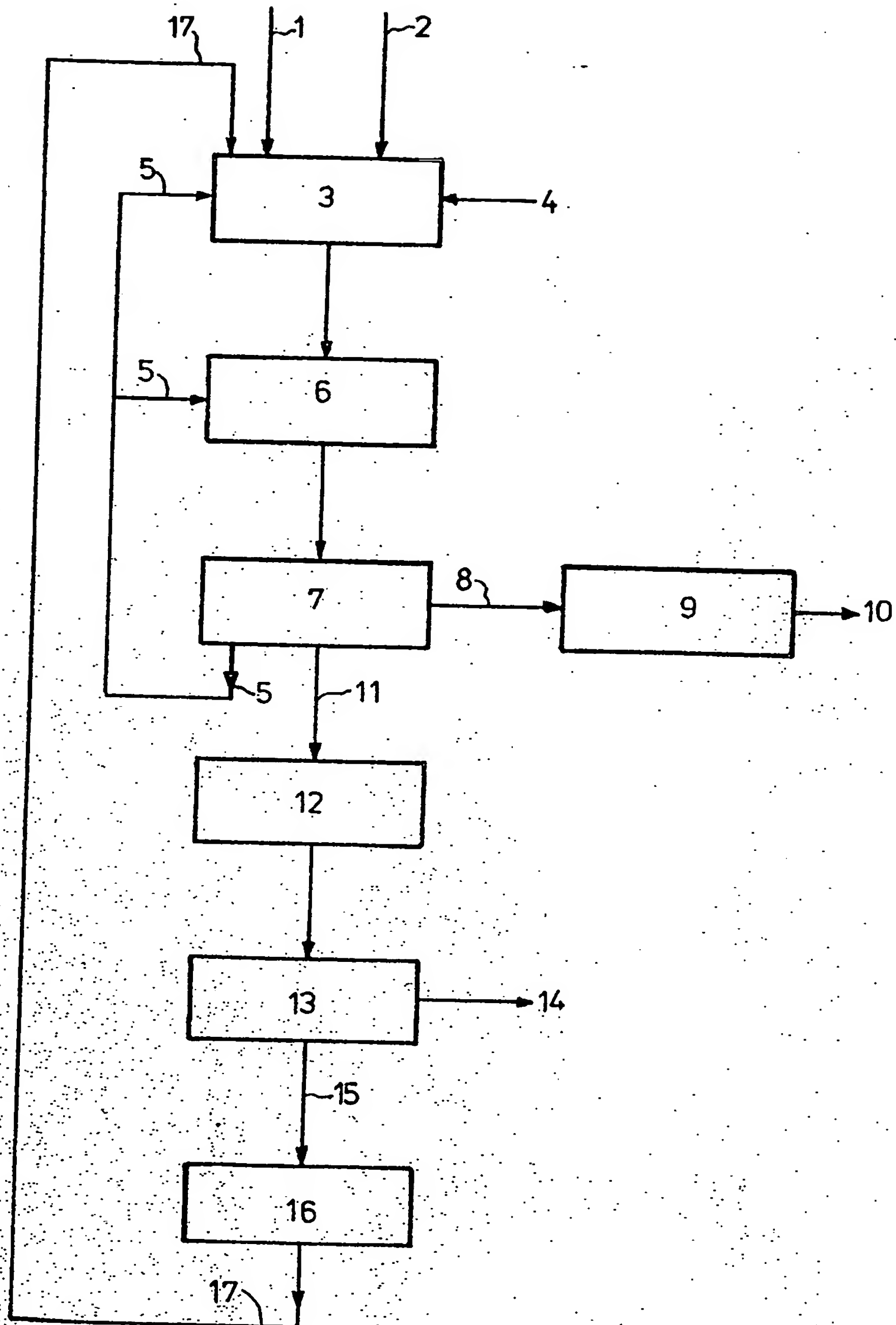
5. A process according to claim 1, 2 or 3, wherein the digestion reaction is initiated by addition of hot 76 to 87% sulphuric acid ("recycled acid") at from 100 to 160°C.
6. A process according to claim 1, 2 or 3, wherein the concentration of the sulphuric acid is between 87 and 91% H_2SO_4 (calculated as solids-free and salt-free acid) at the beginning of the digestion reaction and from 35 to 70% of the sulphuric acid required is recovered from the process as recycled acid.
7. A process according to claim 1, 2 or 3, wherein the concentration of the sulphuric acid is between 88 and 90% H_2SO_4 (calculated as solids-free and salt-free acid) at the beginning of the digestion reaction and from 35 to 70% of the sulphuric acid required is recovered from the process as recycled acid.
8. A process according to claim 1, 2 or 3, wherein the production of the 76 to 87% acid from 60 to 75% pre-concentrated sulphuric acid is effected by evaporation at from 120 to 190°C and from 40 to 150 mbar.
9. A process according to claim 1, 2 or 3, wherein the production of the 76 to 87% acid from 60 to 75% pre-concentrated sulphuric acid is effected by evaporation at from 120 to 190°C and from 40 to 150 mbar and a horizontal evaporator with a tantalum heat exchanger is used as evaporator.
10. A process according to claim 1, 2 or 3, wherein the production of the 76 to 87% acid from 60 to 75% pre-concentrated sulphuric

acid is effected by evaporation at from 120 to 190°C and from 40 to 150 mbar and a circulation evaporator is used as evaporator.

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